

MODELING OF THE THERMAL LOADS AND ENERGY CONSERVATION IN HYDRPONICS SPROUTS PRODUCTION SYSTEMS

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ABSTRACT

Sprouting green fodder production systems (SGFPS) are considered highly condensed agro-industrial systems in terms of electric energy consumption. Therefore, price rising or scarcity of electric energy of the traditional source “Public Network of Electricity” constitutes critical issue in the SGFPS management. Additionally, engineering criteria to determine the technical specifications of suitable electric solar system (ESS) as an alternative source of energy are not found. Therefore, the research main objectives were to construct mathematical model, to determine the thermal loads, to determine the best alternatives of energy conservation, and to develop an engineering criteria to specify suitable ESS. To execute these objectives a mathematical model was constructed and used in the determination of type and quantity of the thermal loads. Statistical trial was designed and executed to determine the best alternative for energy conservation. Engineering criteria were developed to determine the technical specifications of the ESS. The results showed that: The mathematical model is valid to use. The thermal equilibrium is going for cooling direction. The cooling loads are located between 5915.3 and 7739.9 BTU/h. The thermal properties of the building materials are responsible on saving 65% of the thermal loads. Operations management is responsible on saving 35% of the thermal loads, and the engineering criteria should be effective in order to determine the technical specifications of the electric solar energy source to reduce the reliance on conventional source “Public Network of Electricity” (PNE).

Keywords: *Mathematical modelling - thermal loads - materials thermal properties – thermal emissions coefficients - operations management - energy conservation - engineering criteria - electric solar system.*

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1- INTRODUCTION

Production systems of hydroponics sprouted green fodder are considered closed agro-industrial systems. These systems consume a great amount of energy through washing, soaking, cultivation, lighting, ventilation, irrigation, fertigation, cooling, and heating subsystems. Due to decreasing supply and increasing demand on energy, the energy price is continuously going up. Therefore, conservation of utilized energy in the sprouted green fodder production is considered critical issue. As a result, the main objective of this research was to minimize the consumed energy with keeping on quality and quantity of the sprouted green fodder production. To achieve this objective, construction of a mathematical model for determining the utilized energy in sprouted green fodder production is needed. The sprouted green fodder production chambers are constructed as part of residential buildings or a type of greenhouses. Therefore, all equations of energy balance in the residential buildings and the greenhouses could be used as a guide in the construction processes of the energy model.

Energy sources constitute one of the most important factors in wealth generation, economic growth and social development, therefore design and material selection of walls, roofs, ground floors and windows are considered critical issues in energy saving, **Onwuka, O. 2013**. Discouraging of energy consumption in the agricultural sector might increase costs of production activities. At the same time, it minimizes the environmental impact due to reduction of GHGs emissions, **Kempen and Kraenzlein 2008**.

The consumed energy for providing fresh water and cooling the environment of greenhouse constitute a critical issue. This energy could be generated by a sustainable greenhouse system SGH if a computational model was constructed for aiding in the SGH design and determine its limitations, **Farrell et al. 2017**. Significant investments on water and energy are required to limit the negative effects of drought on crop yield, **Zhang et al. 2017**. The agricultural residues are utilized to produce electricity and solid, gaseous and liquid biofuels through bioenergy

technologies, **Song et al. 2015**. A control method of greenhouse heating using computational fluid dynamics (CFD) and energy prediction model (EPM) is used to reduce the energy consumption of agricultural greenhouses, **Chen et al. 2015**. The most effective opportunity for energy conservation in greenhouses is the “Double thermal screen” and “Double glazing” which gives 60% reduction in energy demand, **Vadiee and Martin 2014**. Saving energy in greenhouses is an important issue for growers. Optimal control techniques can be used to minimize energy input for heating, cooling, ventilating, and the injection of industrial CO₂, **Van Beveren et al. 2015a**. Using the delivered heat, CO₂, and rain water from the building in rooftop greenhouse could save 341.93 kWh/m²/yr, **Nadal et al. 2017**.

Using a dynamic photovoltaic (PV) generates “(102W/m²) at shading percentage (78%)” of electric energy which could be used in greenhouse operations management, **Marucci and Cappuccini 2016**. The estimated total energy input and energy productivity for greenhouse cucumber production were estimated as 148836.76 MJ ha⁻¹ and 0.80 kg MJ⁻¹ respectively, **Mohammadi and Omid 2010**. The performance of the heat pump for maintaining the greenhouse air at a day temperature of 27 °C and night temperature of 18 °C with a relative humidity of 40% spans 1.2–4.0 and 1000–16,000 kJ/kg for the Coefficient of Performance (COP) and the Specific Energy Consumption (SEC), respectively, **Chou et al. 2004**. A dynamic optimization system based on optimal control theory was designed for saving energy and maintaining air temperature, and fixing relative humidity inside a modern rose greenhouse, **Van Beveren et al. 2015b**.

The calculation processes of the overall energy balance in flower greenhouses include the balances of heating, radioactive and energy required to sweat, evaporation, sensible heat of air and soil as well as the stored energy in the assimilates formation process through photosynthesis processes, **Ciprian, and Brătucu 2014**. Greenhouse energy balance includes soil surface energy balance, interior air energy balance, and energy balance of the cover, **Mesmoudi et al. 2010**. The heating and cooling Heating Ventilating and Air Conditioning (HVAC) system in combination

with shading of glazing surfaces, controlling windows opening, and forcing convection of external air constitute an innovative plant solution for energy saving in greenhouses, **Priarone et al. 2017**. For energy conservation, simulation model was developed to design new buildings ensuring reduction of consumed energy in heating, cooling, lighting and ventilation process, **Andarini 2014**. Adoption of the net zero energy balance “using an on-site renewable energy source” for heating, domestic hot water, and ventilation in new building is considered an effective way for saving energy, **Hall et al. 2014**.

Nearly Zero Energy Buildings (ZEB) will be one of the main directions for minimizing energy consumption in Europe starting from the end of 2020. ‘Nearly ZEB’ can be achieved by both the maximization of energy efficiency and by using renewable energy sources, **Scognamiglio and Røstvik 2012**. Saving energy could be executed through the use of semi-transparent photovoltaics (STPV) greenhouse system covered with STPV cladding material to transmit daylight, provide some shading and generate solar electricity, **Bambara and Athienitis 2015**. Biogas production provide climate-neutral methane gas, which is used as energy source in the hydroponics systems, **Morken et al. 2015**. Leadership in Energy and Environmental Design (LEED) green building certification label is a tool for saving energy and environmental conservation, **Scofield 2013**. Energy saving needs to take measures for replacing electric heaters with gas boilers, replacing screw chillers with centrifugal chillers, and using energy-saving lamps, **Wang et al. 2016**.

Ground surface temperature in Egypt ranges from 18.36 to 19.38 0C which depends on soil depth, **Serageeldin et al. 2015**. Heating load and cooling load expressions are related to the amount of energy “heat” that would need to be added to or removed for maintaining the room temperature at an acceptable level, **Burdick, A. 2011, Yadav et al. 2.17 and Cheng et al. 2018**.

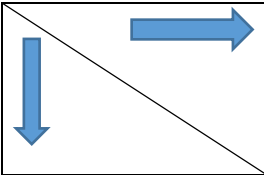
2-MATERIALS AND METHODS

2-1-Trail Design: Complete randomize block design trial with six treatments were statistically designed, table (1). Three shifts for servicing and two systems for cultivating were applied in the trial to study the

consumed energy. Grains washing, soaking, composting and cultivation, sprouting follow up and green fodder harvesting were applied in three shifts which were as follows (8ap-4pm, 4pm-12pm, and 12pm-8am) respectively. Soilless culture and agricultural residues media (rice straw) were used as cultivation media. Treatment number one was used as control for statistical analysis processes.

Copper’s nutrients solution with concentration of 2000 ppm was used, **Trejo-Téllez and Gómez-Merino 2012**. Air temperature and relative humidity were automatically fixed inside the utilized hydroponics green fodder chamber within 20C⁰ and 75% respectively, **Hegab 2018a**. Irrigation scheduled were fixed at 60, 45 and 30 second per 6 hours the first 4 days, the second 4 days, and the third 4 days of the growth cycle respectively, **Hegab 2018b**. Intensity of light (3600lm/m²) through 12/h.day (in exception of the first three days) was used, **Hegab 2018c**.

Table 1: Energy balance trial design:

	<u>Timing of Services</u>			
	<u>Cultivation Systems</u>	First shift (8ap-4pm)	Second shift (4pm-12pm)	Third shift (12pm-8am)
1-Soilless culture	T ₁	T ₂	T ₃	
2-Agric. residues media	T ₄	T ₅	T ₆	

To study energy balance, thicknesses, external and internal temperature (T_{in} and T_{out}) “°C” were measured for the chamber’s walls, windows, doors, ground and roof. Additionally, standard values of technical factors and coefficients were used to complete the energy calculation processes. Consumed energy (CE) “J” were mathematically calculated and

statistically analyzed for the six treatments. The technical criteria of the sprouted green fodder were laboratory measured and statistically analyzed **Hegab 2018c**.

2-2-Mathematical Model Construction:

$$M_a C_a \frac{dT_t}{dt} = \sum Q_{gain} - \sum Q_{loss} \tag{1}$$

where: M_a is isothermal math of air (kg), C_a is specific heat of air (J/kg.°C), T_t is the chamber temperature (°C), t is time (second), Q_{gain} is thermal energy gains inside the chamber (J/s), Q_{loss} is thermal energy lost to the surrounding by air (J/s), **Icorpora et al. 2007**.

Mathematically, the thermal energy balance inside the chamber could be executed when dT_t is equal to zero. Therefore, the value of thermal energy gain and the value of thermal energy lost are equals as follows:

$$\sum Q_{gain} = \sum Q_{loss} \tag{2}$$

In summer season or hot countries, average of the outside air temperature is greater than the inside air temperature. Therefore, the accumulation of energy and increasing air temperature inside the chamber are remarked. Irreversibly, in winter season or cold countries, average of the outside air temperature is less than the inside air temperature on average. Therefore, the losses of energy and decreasing air temperature inside the chamber are remarked. Mathematically, the equation of energy balance inside the chamber could be expressed as follows:

$$\begin{aligned} \sum Q_{gain} = & Q_{walls} + Q_{windows} + Q_{doors} + Q_{roof} + Q_{ground} + Q_{groundedgt} \\ & + Q_{lobors} + Q_{ventilation} + Q_{light} + Q_{irrigation} + Q_{socking} + Q_{harvesting} + Q_{shem} \end{aligned} \tag{3}$$

$$Q_{walls} = \frac{(t_{owa} - t_{iwa})(A_{wa})}{\frac{1}{h_{owa}} + \sum_{jwa=1}^l \frac{b_{jwa}}{k_{iwa}} + \frac{1}{h_{iwa}}} \tag{4}$$

where: Q_{walls} energy gains through the chamber’s walls (w) or (J/s), t_{owa} is air temperature outside the wall (°C), t_{iwa} is air temperature inside the wall

(°C), A_{wa} is the total area of the wall (m²), h_{owa} is the outside convection heat transfer coefficient (W/m².k), b_{jwa} is the thickness of the layer No. j in the wall (m), and k_{jwa} is the thermal conductivity of the layer No. j in the wall (W/m.k), and (h_{iwa}) is the inside convection heat transfer coefficient (W/m².k), **Icorpora et al. 2007, Ciprian and Brătucu 2014, Mesmoudi et al. 2010.**

$$Q_{windows} = \frac{(t_{owi} - t_{iwi})(A_{wi})}{\frac{1}{h_{owi}} + \sum_{jwi=1}^m \frac{b_{jwi}}{k_{iwi}} + \frac{1}{h_{iwi}}} \quad (5)$$

where: $Q_{windows}$ energy gains through the chamber's windows(w) or (J/s), t_{owj} is air temperature outside the window (°C), t_{iwj} is air temperature inside the window (°C), A_{wi} is total area of windows (m²), h_{owi} is the outside convection heat transfer coefficient (W/m².k), b_{owa} is the thickness of the layer No. j in the window m, k_{jwa} is the thermal conductivity of the layer No. j in the window (W/m.k) and h_{iwi} is the inside convection heat transfer coefficient (W/m².k), **Icorpora et al. 2007, Wang 2016.**

$$Q_{doors} = \frac{(t_{odo} - t_{ido})(A_{do})}{\frac{1}{h_{odo}} + \sum_{jdo=1}^l \frac{b_{jdo}}{k_{ido}} + \frac{1}{h_{ido}}} \quad (6)$$

where: Q_{doors} energy gains through the chamber's doors(w) or (J/s), t_{awj} is air temperature outside the door (°C), t_{ido} is air temperature inside the window (°C), A_{wi} is area of doors (m²), h_{odo} is the outside convection heat transfer coefficient (W/m².k), b_{ido} is the thickness of the layer No. j in the door m, k_{jdo} is the thermal conductivity of the layer No. j in the door (W/m.k) and h_{ido} is the outside convection heat transfer coefficient (W/m².k), **Icorpora et al. 2007, Bambara and Athienitis 2015.**

$$Q_{roof} = \frac{(t_{aro} - t_{iro})(A_{ro})}{\frac{1}{h_{oro}} + \sum_{jro=1}^o \frac{b_{jro}}{k_{jro}} + \frac{1}{h_{iro}}} \quad (7)$$

where: Q_{roof} energy gains through the chamber's roof(w) or (J/s), t_{aro} is air temperature outside the roof (°C), t_{ido} is air temperature inside the roof (°C),

A_{wi} is area of roof (m^2), h_{oro} is the outside convection heat transfer coefficient ($W/m^2.k$), b_{iro} is the thickness of the layer No. j in the roof (m), k_{jro} is the thermal conductivity of the layer No. j in the roof ($W/m.k$) and h_{iro} is the inside convection heat transfer coefficient ($W/m^2.k$), **Icorpora et al. 2007.**

$$Q_{ground} = \frac{(t_{agro} - t_{igro})(A_{gro})}{\frac{1}{h_{ogro}} + \sum_{jgro=1}^o \frac{b_{jgro}}{k_{jgro}} + \frac{1}{h_{igro}}} \quad (8)$$

where: Q_{ground} energy gains through the chamber's ground (w) or (J/s), t_{agro} is air temperature outside the ground ($^{\circ}C$), t_{igro} is air temperature inside the ground ($^{\circ}C$), A_{gro} is area of ground (m^2), h_{ogro} is the outside convection heat transfer coefficient ($W/m^2.k$), b_{igro} is the thickness of the layer No. j in the roof (m), k_{jgro} is the thermal conductivity of the layer No. j in the roof ($W/m.k$) and h_{igro} is the inside convection heat transfer coefficient ($W/m^2.k$), **Icorpora et al. 2007.**

$$Q_{linear} = (l_{gr})(\Psi_{gr})(t_{ogr} - t_{igr}) \quad (9)$$

where: Q_{linear} linear energy gains (w) or (J/s), l_{gr} is length of the intersection line (m), Ψ_{gr} is the linear head losses through the ground ($W/m.k$), t_{ogr} is air temperature outside the chamber ($^{\circ}C$), and t_{igr} is air temperature inside the chamber ($^{\circ}C$), **Barbosa et al. 2015, Ahmad et al. 2010.**

$$Q_{labors} = (500 / 2.16)(LN)(WR) \quad (10)$$

where: Q_{labors} energy gains from labors activities (w) or (J/s), and LN is labor number inside the chamber (w), and WR working rate (hour/day).

$$Q_{ventilation} = \frac{(ACH_a)(V_a)}{3600}(C_a)(\rho_a)(t_{oa} - t_{ia})(1 - \eta) \quad (11)$$

where: $Q_{ventilation}$ energy gains through the chamber ventilation (w) or (J/s), ACH_a is chamber air change per hour, V_a is volume of chamber (m^3), C_a is specific density of air (kg/m^3), ρ_a is specific heat of air ($J/kg.k$), t_{oa} is air temperature outside the chamber ($^{\circ}C$), t_{ia} is air temperature inside the chamber ($^{\circ}C$), η is ratio of the leaving air to recovered air, **Ahmad et al. 2010.**

$$Q_{light} = LI * A_{ch} * HGC \quad (12)$$

where: Q_{light} energy gains from the chamber lighting (w) or (J/s), LI is light intensity (lm/m²), A_{ch} is chambers area (m²), HGC is heat generation coefficient of light 'depends on light source' (w/lm), **Ahmad et al. 2010 and Uddin et al. 2012.**

$$Q_{irrigation} = \frac{(AWH_{ir})(V_{ir})}{3600} (C_{ir})(\rho_{ir})(t_{oir}-t_{iir}) \quad (13)$$

where: $Q_{irrigation}$ energy gains through the irrigation process (w) or (J/s), AWH_{ir} is irrigation process number per hour, V_{ir} is volume of irrigation water per process (m³), C_{ir} is specific density of water (kg/m³), ρ_{ir} is specific heat of water (J/kg.k), t_{oir} is water temperature outside the chamber (°C) and t_{iir} is water temperature inside the chamber (°C), **Ahmad et al. 2010.**

$$Q_{socking} = \frac{(AWH_{sg})(V_{sg})}{3600 * 24} (C_{sg})(\rho_{sg})(t_{osg}-t_{isg}) \quad (14)$$

where: $Q_{socking}$ energy gains through grains socking process (w) or (J/s), ACH_{sg} is socking process number per day, V_{aw} is volume of socked grains (m³), C_{sg} is specific density of the socked grains (kg/m³), ρ_{sg} is specific heat of the socked grains (J/kg.k), t_{osg} is socked grains temperature outside the chamber (°C), and t_{isg} is socked grains temperature inside the chamber (°C), **Ahmad et al. 2010.**

$$Q_{harvesting} = \frac{(AWH_{gf})(V_{gf})}{3600} (C_{gf})(\rho_{gf})(t_{ogf}-t_{igf}) \quad (15)$$

where: $Q_{harvesting}$ energy losses through the green fodder harvesting (w) or (J/s), ACH_{gf} is socked grains number per day, V_{gf} is volume of green fodder per process (m³), C_{gf} is specific density of the green fodder (kg/m³), ρ_{gf} is specific heat of the green fodder (J/kg.k), t_{ogf} is green fodder temperature outside the chamber (°C), t_{igf} is green fodder temperature inside the chamber (°C), **Ahmad et al. 2010.**

$$Q_{shem} = 0.75 * 1000(HP / Emef) * Fu * Fp * CLF_{-h} \quad (16)$$

where: Q_{shem} is the sensible heat gain from electric motor, (W) or (J/s), Fu is usage factor (%), Fp is part of load operating factor for motor type (%),

HP is rated electrical horsepower of equipment motor (1kW = 0.75 HP), *Emef* is electric motor Efficiency (%), and *CLF_{-h}* is cooling Load Factor (CLF) for given hour, **Thomas 2017**.

2-3-Model Solving: Equations form number (4) to (16) are considered details of all components in the right side of the equation number (3). Total value of these equations “from (4) to (16)” express on energy gain inside the chamber or energy loss outside the chamber through the sprouting and growth operations. Since, all the terms of these equation “in exception of temperature” are considered constant for each case study “Chamber”. Therefore, the computing program runs one loop only to determine the value of this constant which will be kept in the computer memory. Systematically, the energy balance is determined by the program through multiplying this constant in the temperature differences at each point of measuring time.

3-RESULTS AND DISCUSSIONS

3-1-Sprouting chamber and heat balance direction: Since the ideal air temperature T_{db} for sprouting and growth processes is 20°C. The recoded air temperature T_{db} outside the chamber is above the ideal temperature, as shown in table (2). Therefore, the accumulated thermal loads inside the chamber must be removed outside through air cooling process for maintaining the chamber temperature at the acceptable range “20°C”. Clearly, the chamber heat balance direction is to remove the excessive heat from the inside to the outside space. Through the winter season, the differences between the recoded and the acceptable temperature T_{db} were approximately steady at 4°C from 0 to 9am, increase from 9 and 11°C through the period from 9 am to 15 afternoon, and decrease from 11 to 4°C through the period from 15 afternoon to 21 am. Through the spring season, the differences between the recoded and the acceptable temperature T_{db} approximately steady at 9°C from 0 to 9am, increase from 10 and 17°C through the period from 9 am to 15 afternoon, and decrease from 17 to 9°C through the period from 15 afternoon to 21 am. Through the summer season, the differences between the recoded and the acceptable temperature T_{db} were approximately steady at 14°C from 0 to 9am, increase from 14 and 22°C through the period from 9 am to 15 afternoon, and decrease from

22 to 14°C through the period from 15 afternoon to 21 am. Through the winter season, the differences between the recoded and the acceptable temperature T_{db} approximately steady at 10°C from 0 to 9am, increase from 11 and 18°C through the period from 9 am to 15 afternoon, and decrease from 18 to 10°C through the period from 15 afternoon to 21 am. According to these data, this climate is considered moderate free of frost and its bad effects on the agricultural production. This result agrees with **El-Ramady et al. 2013 and Hussein and Mohamed 2016.**

Table (2): External air temperature T_{db} (°C).

		Measuring time (h) within the day							
		0	3	6	9	12	15	18	21
Winter	R_1	23	24	24	24	30	33	27	26
	R_2	26	25	23	25	32	32	29	25
	R_3	26	23	22	23	31	34	28	24
	\bar{Y}	25	24	23	24	31	33	28	25
Spring	R_1	30	29	30	31	33	37	31	30
	R_2	29	28	29	30	36	38	32	29
	R_3	28	27	28	29	36	36	30	28
	\bar{Y}	29	28	29	30	35	37	31	29
Summer	R_1	35	34	31	33	39	43	36	35
	R_2	33	32	34	35	40	42	37	33
	R_3	34	33	34	34	41	41	38	34
	\bar{Y}	34	33	33	34	40	42	37	34
Autumn	R_1	29	30	31	32	34	40	34	30
	R_2	33	29	30	31	35	37	31	30
	R_3	29	28	29	30	33	37	31	30
	\bar{Y}	30	29	30	31	34	38	32	30

where: R is replicates of temperature measurements, R_1 , R_2 , and R_3 are three days (selected in randomization) within each season, and \bar{Y} is mean of replicates.

3-2- Values and behaviors of cooling loads: Table (3) shows vales of cooling loads (BTU/h) at eight stations through the day hours (24h) for the four seasons. The cooling load values are 3551.6 and 5741.3 (BTU/h) at 0 and 15 h for the winter season, 4659.2 and 6728.4 (BTU/h) at 0 and 15 h

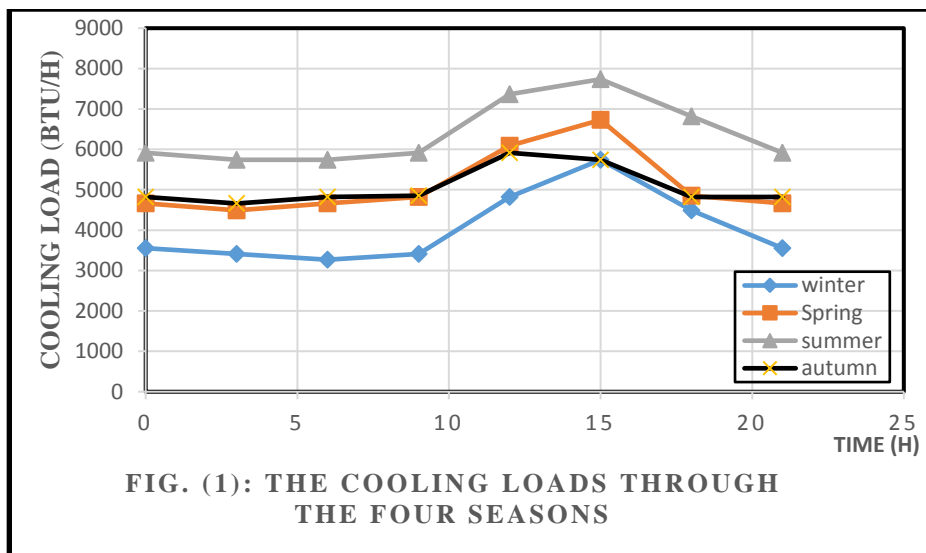
for the spring season, 5915.3 and 7735.9 (BTU/h) at 0 and 15 h for the summer season, and 4819.8 and 5741.3 (BTU/h) at 0 and 15 h for the autumn season. As a result, the minimum cooling load was found at midnight of winter season (3551.6BTU/h or 0.296Ton or 1.396hp), and the maximum cooling load was found at 15 pm afternoon of summer season (7735.9BTU/h or 0.654Ton or 3.04hp). These results are logic, since the outside air temperature reaches the minimum degree at 1 midnight. Irreversibly, the outside air temperature reaches the maximum degree at 1 afternoon. This result agrees with **Bellos et al. 2015 and Cheng et al. 2018.**

Table (3): Sprouting chamber cooling loads (BTU/h):

	Time, hour							
	0	3	6	9	12	15	18	21
Winter	3551.6	3409.6	3267.5	3409.6	4819.8	5741.3	4489.5	3551.6
Spring	4659.2	4489.5	4659.2	4819.8	6089.2	6728.4	4849.8	4659.2
Summer	5915.3	5741.3	5741.3	5915.3	7367.5	7735.9	6814.6	5915.3
Autumn	4819.8	4659.2	4819.8	4849.8	5915.3	5741.3	4819.8	4819.8

$$1(\text{J/s}) = 3.412(\text{BTU/h}), 12000(\text{BTU/h}) = 1\text{Ton and } 1\text{Ton} = 4.716 (\text{hp})$$

The remarked behavior of the cooling load curves through the four season are approximately similar, Fig. (1). The summer cooling load curve was found at the highest level. The winter cooling load curve was found at the lowest level. Both the autumn and the spring curves were found at the middle. The remarked trend of each one of the cooling load curves is approximately horizontal through the period from 0 to 9h, up to top from 9 to 15h and top to down from 15 to 24h. This behavior is attributed to the same change in the outside air T_{db} . Since the outside air temperature takes the same trend from 0 to 21h. Therefore, stopping any operation such as “door opening, window opening, production harvesting, grain cultivation, sprouts irrigation, and production servicing” are considered critical issue in energy conservation. This must be done to prevent the outside hot air from entering to the chamber. This concept agrees with the heat transfer equations “convection case” that were mentioned in the heat transfer textbooks such as **Icorpora et al. 2007.**



3-3-Energy conservation: Saving the consumed energy in sprouting system could be done through two stages. The first is the design and construction stage which determine types and dimensions of the building materials. The second is the engineering management stage of the technical operations inside the SGFPS.

In dealing with the first stage, table (4) shows the share percentages of heat sources through the four seasons. These percentages slightly change from season to another depending on the changes in the outside air temperatures T_{ab} . Since the outside temperature is out of control, therefore it is impossible to stabilize the cooling load through the four seasons. Additionally, Fig. (2) shows values of mathematical means for share percentages of each heat source accumulated inside the chamber. Through the first stage “design and construction” the accumulated heat inside the chamber passing through walls, doors, windows, roofs, and ground could be minimized which depends on the right selection of heat transfer coefficient ($W/m^2.k$), thermal conductivity ($W/m.k$), thickness (m), specific density (kg/m^3), and specific heat ($J/kg.k$) of the utilized materials. The heat production from equipment and lighting system could be minimized by using equipment and lighting system with low thermal emission factor BTU/kW. This concept agrees with the heat transfer equations that were mentioned in the heat transfer textbooks such as **Icorpora et al. 2007.**

In dealing with the second stage, management of the technical operations such as “grain cultivation, production harvesting, production servicing which need to open doors and windows” have great effect on the cooling load value and energy saving. Fig. (2) shows the share percentages of heat sources in cooling load. Total values of share percentages of the technical operations which were mentioned above constitute 36.91% of the total cooling loads. These loads could be saved through management of the technical operations. Table (5) shows statistical analysis results of factorial experiment containing six treatments of operations management. The smallest cooling load was found by executing the technical operations through the third shift (**12 midnight-8am**) with cultivation on agricultural residues. The greatest cooling load was found by executing the technical operations through the first shift (**8am-4pm**) with soilless cultivation. Statistically, the difference between the smallest and the greatest cases is highly significant at $P \leq 0.05$. According to the values of least significant difference LSD, the other treatments were statistically ranked between the two cases. Mathematically, the right management of the technical operations save 29.24% of the total cooling loads. This result is logic since achieving the technical operations at the first shift gives a great chance to the hot air to enter the chamber. Irreversibly, achieving the technical operations at the third shift gives a great chance to the cold air to enter the chamber.

3-4-Renewable energy source and its engineering criteria: Due to the limitation of electric energy in the conventional source, therefore using renewable sources such as solar energy in the SGFPS is obligatory. Technically, the required energy for air cooling, air ventilation, lighting, and irrigation and fertigaion loads must be covered. Mathematically, these loads could be expressed though the general criteria as follows:

$$E_{UA} = (E_{Ost}) / V_{Ch} \quad 17$$

$$E_{UA} = (E_{Cl} + E_{Av} + E_{Li} + E_{Ir}) / V_{Ch} \quad 18$$

Where: E_{UA} is the energy consumption per cubic meter of chamber's volume kWh/m³, E_{Ost} is sum of loads that could be operated at the same time per cubic meter of chamber's volume kWh/m³. V_{Ch} is the chamber

volume m^3 , E_{CL} , E_{AV} , E_{Li} and E_{Ir} are cooling, air ventilation, lighting, and irrigation loads kWh, respectively.

Due to the limitation of the traditional sources for electric energy, therefore using renewable energy sources such as electric solar system is advisable. Technically, the electric solar system consists of electric panels, DC to AC inverter, charge controller, and batteries. The electric solar panels are considered the corner stone in the electric solar system. Mathematically, the needed panels could be expressed as follows:

$$NP = (E_{AU} \times V_{Ch}) / E_{pa} \quad 19$$

$$NP_{Ro,Array} = E_{vo} / P_{vo} \quad 20$$

$$NR_{Array} = PN / NP_{Ro,Array} \quad 21$$

$$NB = E_{AU} / B_{cap} \quad 22$$

where: NP is number of the needed panels “Modules”, E_{pa} is the generated energy per panel kWh, $NP_{Ro,Array}$ is number of panels “Modules” per each row in the panels array, P_{vo} is voltage per panel, NR_{Array} is number of rows per array, NB is number of storage batteries, and B_{cap} is battery capacity kWh.

3-5- Confirmation by Case Study: The air cooling load is found between 4524.08 and 6393.33 BTU/h on average. The air ventilation load is found between 1474.04 to 2948.08 BTU/h in average. The lighting load is found between 1364.86 to 1706.07 BTU/h on average. The irrigation and fertigaion load is found between 2559.11 to 3412.14 BTU/h on average. Technically, the total loads which could be operated at the same time are located between 9922.09BTU/h (2.91kW) and 14456.62 BTU/h (4.241kW) on average, **Equations 17-18**. Since the total volume of the chamber is $72m^3$, therefore the total loads per cubic meter are located between $137.81BTU/h.m^3$ ($0.04kW/m^3$) and $200.79BTU/h.m^3$ ($0.06kW/m^3$) on average, **Equation 17-18**. The electric panels “Modules” are found in Egypt with dimensions of 99 and 164cm for Monocrystalline or Polycrystalline Silicon. These panels generate electricity with Voc. of 37.5 V and current of 8.75 Ampere. Array of panels (3 rows 6 panels in each row) generates DC electricity 4.5 kWh with 225V and 26.25A, **Equation 19**. The needed number of solar electric storage batteries is 4 with specs of 12V at 1000 AH, **Equations 19-22**.

Table (4): Energy sources and its share percentages in cooling loads within the four seasons:

	Cooling load (%)													Total (%)
	Q_{walls}	Q_{windo}	Q_{door}	Q_{roof}	$Q_{grou.}$	Q_{linear}	Q_{labor}	Q_{light}	$Q_{ventl.}$	$Q_{irrig.}$	$Q_{cult.}$	$Q_{harv.}$	Q_{shen}	
Winter	16.51	2.44	6.59	9.41	2.77	4.99	13.33	15.45	10.55	8.33	3.85	2.94	2.84	100
Spring	18.75	3.65	5.85	9.41	3.89	5.91	9.11	14.45	9.88	9.43	3.31	3.86	2.50	100
Summer	20.31	4.81	4.61	7.05	2.56	6.36	7.77	12.85	7.38	10.51	4.52	6.79	4.48	100
Autumn	19.35	3.63	5.94	9.41	3.12	4.43	9.94	14.45	8.45	9.95	3.63	4.85	2.85	100
Average	18.74	3.63	5.74	8.82	3.08	5.43	10.04	14.31	9.06	9.55	3.82	4.62	3.16	100

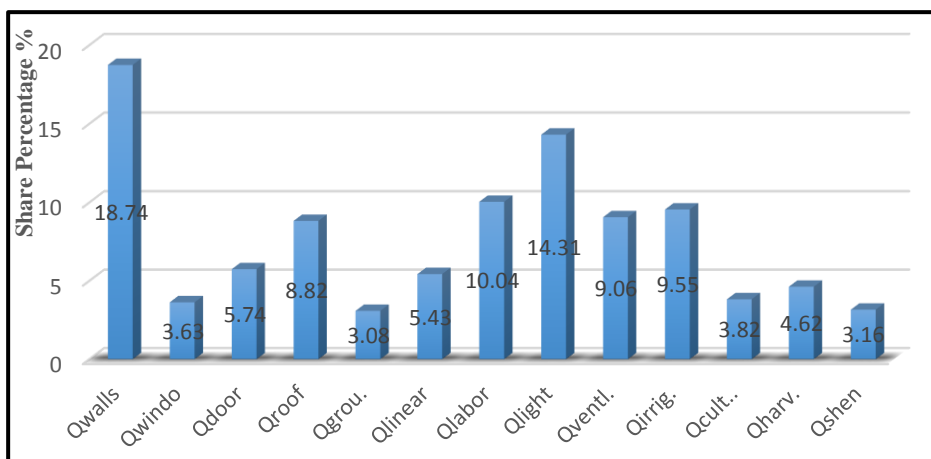


Fig. (2): Average of share percentages of the heat sources in the sprouting chamber.

Heat Sources

Table (5): Operations timing and its effect on cooling loads (BTU/h):

	<u>Timing of operations</u>		
	<u>Cultivation Systems</u>	First shift (8ap-4pm)	Second shift (4pm-12)
1-Soilless culture Control	6393.33	5719.33 ^c	5130.10 ^b
2-Agric. residues media	5614.67 ^c	5095.46 ^b	4524.08 ^a

where: The letters (a, b and c) indicate to means of cooling loads replicates which are homogenous and significantly different at $P \geq 0.05$.

4- CONCLUSIONS

For the purposes of application, the research results mentioned above could be concluded in the following points:

- 1- It is necessary to use the constructed mathematical model for determining the quality and quantity of the thermal loads to achieve heat balance inside the SGFS.
- 2- It is necessary to select building materials with low thermal coefficients and equipment with low thermal emissions for saving energy. Since the technical specs of the building materials and electric equipment are responsible on saving 65% of the thermal loads.
- 3- It is necessary to finish the technical operations through the period from 1 midnight to 8 am for saving energy. Since the management of the technical operations is responsible on saving 35% of the thermal loads.
- 4- It is necessary to use the developed engineering criteria to determine the technical specs of the SES for reducing the reliance on the PNE.

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الملخص العربي

نمذجة الأحمال الحرارية والحفاظ على الطاقة بمنظومات إنتاج المستنبتات مائياً

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المشكلة: تعتبر منظومات إنتاج الأعلاف الخضراء المستنبتة مائياً منظومات زراعية صناعية كثيفة استخدام الطاقة. حيث يتطلب الحصول على إنتاج جيد إجراء عمليات غسيل ونقع وكمز وزراعة، وري وتسميد، وإضاءة، وتهوية، وتبريد، وحصاد. وأن كل هذه العمليات تتم بواسطة منظومات فرعية أوتوماتيكية تعمل بالطاقة الكهربائية. ولذلك فإن ارتفاع أسعار أو ندرة الطاقة الكهربائية بالمصدر التقليدي مع غياب المواصفات الفنية لمنظومات إنتاج الطاقة المتجددة يعتبر أحد المشاكل الرئيسية في عمليات الإنتاج.

الهدف: ولذلك فإن الهدف الرئيسي من هذا البحث هو (١) بناء نموذج رياضي لتحديد نوعية وحجم الأحمال الحرارية، (٢) تحديد أفضل أساليب الحفاظ على الطاقة خلال مرحلتى التصميم وإدارة الإنتاج، (٣) وضع معايير هندسية تطبيقية وإستخدامها في تحديد المواصفات الفنية لمنظومة إنتاج طاقة متجددة لتشغيل تجهيزات غرف الإستنبتات لتقليل الإعتماد على المصدر التقليدى للطاقة الكهربائية.

المنهج العلمى: لتحقيق الهدف المنشود من هذا البحث تم (١) بناء نموذج رياضي لحساب الأحمال الحرارية داخل غرف إنتاج الأعلاف الخضراء المستنبتة، (٢) استخدام النموذج في حساب وتحديد نوعية الأحمال الحرارية داخل غرفة إنتاج الأعلاف الخضراء المستنبتة، (٣) تحديد أساليب الحفاظ على الطاقة خلال مرحلتى تصميم الغرف وإدارة الإنتاج، (٤) تصميم وتنفيذ تجربة عاملية لتحديد أفضل البدائل لإدارة العمليات الفنية توفيراً للطاقة. إعتمدت العمليات الحسابية الرياضية والإحصائية على بيانات تم الحصول عليها من خلال قياس درجات الحرارة الجافة للهواء خارج وداخل الغرفة مع الإستعانة بجداول الخصائص الحرارية والطبيعية والهندسية لمواد البناء والمعدات والتجهيزات الكهربائية المنشورة على الشبكة العنكبوتية بالمواقع العلمية المتخصصة.

النتائج: توصل البحث من خلال تحليل مخرجات النموذج الرياضى ونتائج التحليل الإحصائى للتجارب العملية الى أن: (١) النموذج الرياضى صالح لحساب الأحمال الحرارية بالمنظومات الحيوية للإنتاج الزراعى، (٢) الإلتزان الحرارى داخل هذه المنظومات يتطلب طرد الحرارة من داخل الغرف الى الخارج على مدار العام، (٣) مجموع أحمال التبريد تتراوح من ٥٩١٥,٣ الى ٧٧٣٩,٩ وحدة حرارية بريطانية لكل ساعة، (٤) توفير جزء كبير من ثلثى أحمال التبريد يعتمد على إختيار مواد بناء ذات معاملات حرارية منخفضة، (٥) توفير ثلث أحمال التبريد يعتمد على موعد إدارة العمليات الفنية داخل الغرف، (٦) خلاصة تحليل النتائج تعد معايير هندسية فى تصميم منظومة الطاقة داخل غرف الإستنبتات، (٧) المعايير الهندسية المستخلصة تطبيقية وتم إستخدامها فى تحديد المواصفات الفنية لمنظومة إنتاج طاقة متجددة لتشغيل تجهيزات غرف الإستنبتات.

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التوصيات: أوصى البحث بالنقاط التالية (١) ضرورة إستخدام النموذج الرياضى فى حساب الأحمال الحرارية بالمنظومات الحيوية للإنتاج الزراعى لتحديد نوعية وحجم الأحمال الحرارية وتوصيف منظومة تهيئة البيئة الداخلية، (٢) ضرورة الإختيار الجيد لمواد البناء بأن تكون ذات معاملات حرارية منخفضة وتجهيزات ومعدات ذات معامل إنبعاث حرارى منخفض، حيث يتوقف على هذا الإختيار ٦٥% من الأحمال الحرارية. (٣) ضرورة إتمام جميع الأعمال الفنية المرتبطة بإدارة الإنتاج خلال الفترة من الساعة الواحدة بمنتصف الليل حتى الساعة الثامنة صباحا، حيث يتوقف على هذا الموعد ٣٥% من الأحمال الحرارية. (٤) ضرورة إستخدام المعايير الهندسية فى تحديد المواصفات الفنية لمنظومة إنتاج طاقة كهربية متجددة لتقليل الإعتماد على المصدر التقليدى للطاقة الكهربائية.